

# Glycol Filtration

**a new application in natural gas  
production plants**

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## TOPICS

- What is Glycol and how is it used ?
- Filtration Requirements for Glycols
- Filter Design Basis and Performance
- Process Flow Diagram
- Conclusion

# What is Glycol and how is it used ?

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Besides Amine Glycol is the second chemical that is used in nearly every natural gas production plant in large quantities. Circulating in a closed loop Glycol is subject to degradation and accumulation of impurities.



*Glycol storage tanks during shipment to STATOIL's new Liquid Natural Gas (LNG) Production Plant in Hammerfest, Norway.*

*The large storage tanks for Lean and Rich Glycol have holding capacities of 3'500 m<sup>3</sup> each and weight around 400 tons.*

# What is Glycol and how is it used ?

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Glycol in the form of MEG or TEG (mono-ethylene-glycol, tri-ethylene-glycol) serves as an antifreeze agent.

Glycol is injected into the wellstream to prevent the formation of ice and blockages in the pipeline carrying raw gas to land.



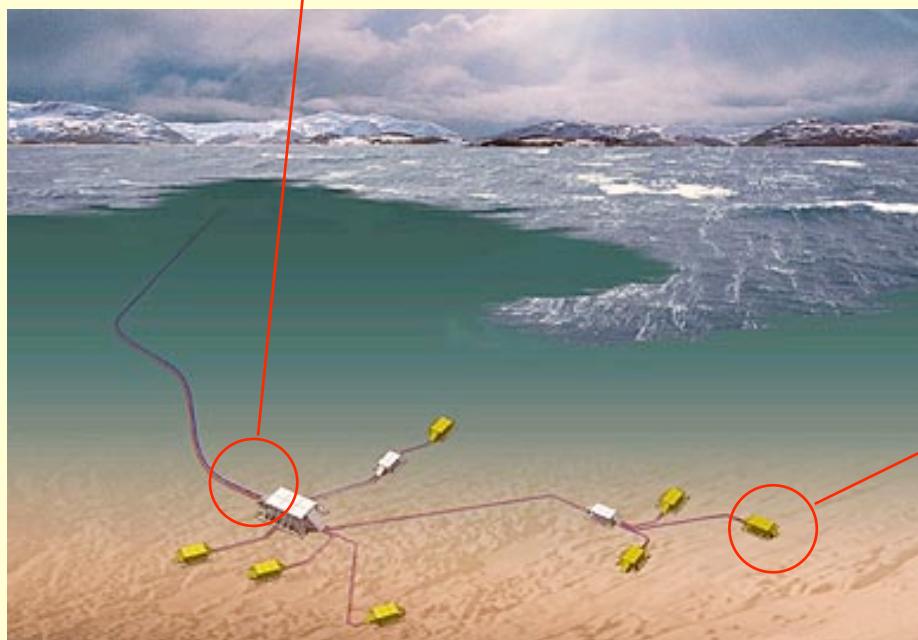
STATOIL's Liquid Natural Gas (LNG) Production Plant near Hammerfest, Norway during construction

# What is Glycol and how is it used ?

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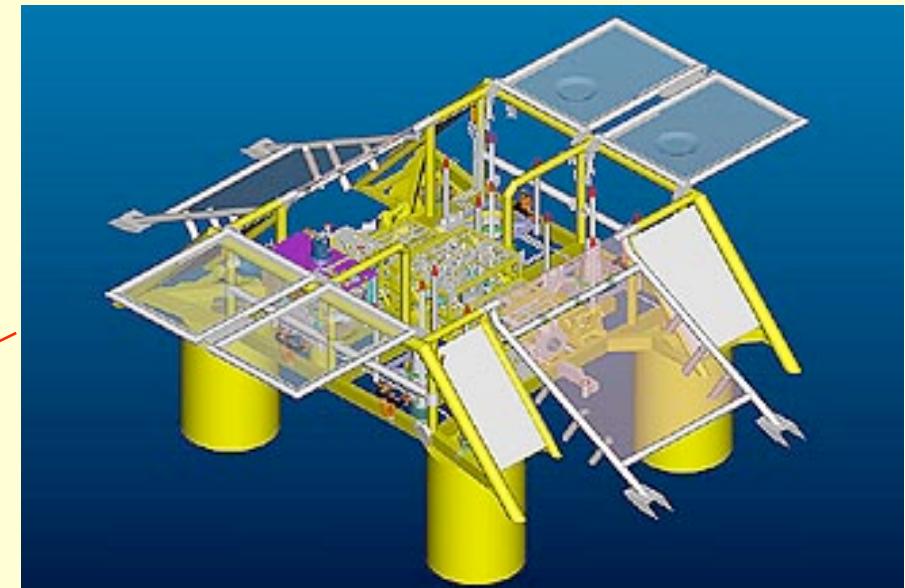


Subsea pipelines & manifolds



Subsea wellheads, pipeline and gas distribution network

**“Rich” glycol arriving on land - after separation of coarse solids (dirt, sand etc.), liquid hydrocarbon and the gas phase - contains fine solid impurities, dissolved HC, dissolved salts and approx. 40 - 50 % water.**



Subsea well platform

# Filtration Requirement for Glycol

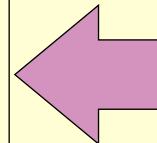
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**Before “Lean” glycol can be send back offshore to the wellhead it must be regenerated in a multi-stage purification process.**

**While dissolved components are removed by adsorption / ion exchange and water is evaporated, fine solids must be filtered out as the first step.**

**Typical solids to be removed:**

- Carbonate Scale  $\text{CaCO}_3$ ,  $\text{MgCO}_3$
- Corrosion  $\text{FeCO}_3$ ,  $\text{FeS}$ ,  $\text{Fe}_3\text{O}_4$
- Very small particle size 1-10  $\mu\text{m}$
- Total solids  $\sim 100\text{-}200 \text{ ppm}$



## Typical Design Values for the Filter System

Required solids recovery rate	99%
Feed Composition in wt%	
H <sub>2</sub> O	42.53
MEG	55.77
CO <sub>2</sub>	234
H <sub>2</sub> S	1
Hydrocarbons	109
Aromates	550
Phenol	625
Salt	0.62
NaOH	0.89
Dissolved Carb.Scale	188
Dissolved Corrosion	49
Carbonate Scale solid	76
Solid Corrosion	83
Flow rate kg/h	15 322 x 1.5
Pressure barg	7
Temperature °C	30
Density kg/m <sup>3</sup>	1051
Viscosity cP	3.8

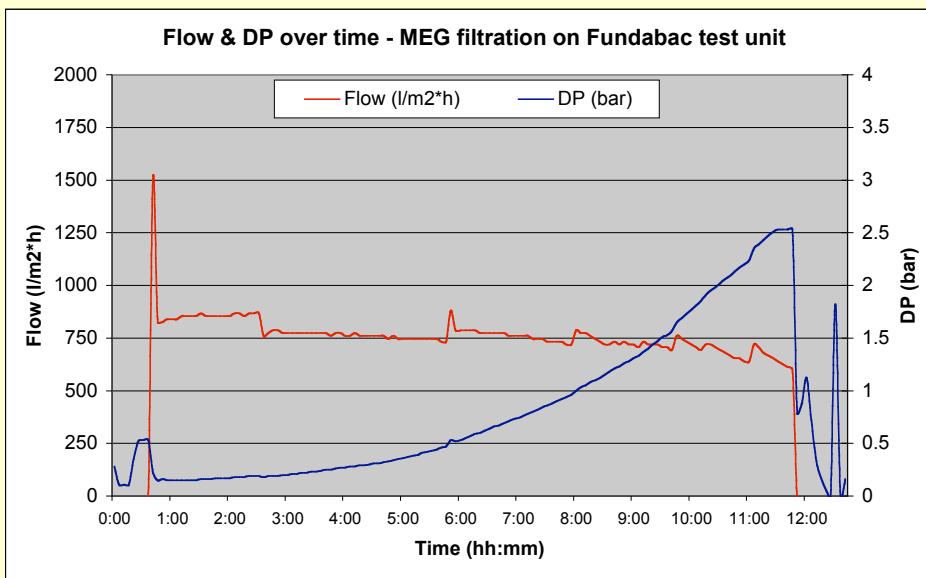
# Filter Design Basis & Performance

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Extensive pilot tests at a site with a 2.7 m<sup>2</sup> FUNDABAC® filter were very successful.

Filter aid as precoat + body feed was necessary to achieve the required filterability and filtrate quality.

DrM designed and quoted the full scale filtration unit - a dual filter skid with 2 x Fundabac R-62 m<sup>2</sup>.



Data from pilot test run

Capacity Case		150%	100%	Remark	
		22983 kg/hr	15322 kg/hr		
1	Continuous filtrate flow	m <sup>3</sup> /hr	21.9 <sup>1)</sup> )	14.6	Note <sup>2)</sup>
2	Continuous feed flow to filter	m <sup>3</sup> /hr	44		Note <sup>3)</sup>
3	Continuous overflow	m <sup>3</sup> /hr	23.1	29.4	Note <sup>3)</sup>
4	Expected duration of the filtration	hr	5	7.5	
5	Suspended solids in feed from Rich MEG storage tank	ppm	200	(design maximum)	
6	Mass flow of suspended solids to filter	kg/hr	4.60	3.06	
7	Required differential pressure across filter towards end of filtration	bar	6.0		
8	Required inlet pressure to filter	barg	7.0	Note <sup>4)</sup>	
9	Suspended solids in treated Rich MEG	ppm	≤1 <sup>1)</sup> )	Note <sup>5)</sup>	
10	Filtration efficiency	%	≥ 99	Note <sup>6)</sup>	
11	Filter aid type for pre-coat		Celite® 545		
12	Filter aid dosage for pre-coat (kg per m <sup>2</sup> filter area)	kg/m <sup>2</sup>	0.75 - 1.0		
13	Filter aid type for body-feed		Celite® 545		
14	Filter aid dosage for body-feed (kg per kg of suspended solids)	kg/kg	2		
15	Total filter aid consumption (kg per kg of removed solids)	kg/kg	5.0 <sup>1)</sup> )		
16	Filter aid content of body-feed slurry	% wt	10		
17	Volumetric flowrate for pre-coating	m <sup>3</sup> /hr	90		
18	Diff. head recomm. for pre-coat pump	m	16	Note <sup>7)</sup>	
19	Volumetric flowrate for body-feed	l/hr	92	61	
20	Dryness of the discharged filter cake	% wt	≥55 <sup>1)</sup> )		

Design figures of full scale unit

16. - 19.09.2004

# Conclusion

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*DrM*  
*Korfu 2004*

**The proposed FUNDABAC® Filter provides significant advantages compared to alternative filtration solutions which were also considered:**

- Considerable savings on operational and waste disposal cost compared to cartridge filters traditionally used in Glycol systems.
- Improved filtration efficiency (70-80% → 99%) compared to decanter centrifuges and savings on slurry disposal cost.
- Reduced Glycol losses.